Solubility of 1-(2-Dimethylaminoethyl)-5-mercapto-1*H*-tetrazole in Water, DMF, Methanol, Ethanol, 1-Propanol, 2-Propanol, 1-Butanol, and 2-Butanol between (293 and 343) K

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The solubility of 1-(2-dimethylaminoethyl)-5-mercapto-1*H*-tetrazole (DMMT) in water, *N*,*N*-dimethylformamide (DMF), methanol, ethanol, 1-propanol, 2-propanol, 1-butanol, and 2-butanol between (293 and 343) K was measured using a laser monitoring observation techinque. The results were correlated with a semiempirical equation, the calculated results of which are proved to show fine representation of experimental data.

Introdution

DMMT ($C_5H_{11}N_5S$, CAS Registry No. 61607-68-9) is a white crystalline powder and a useful chemical for an intermidiate for the synthesis of cefotiam. To determine the proper solvent and design, an optimized crystallization process is necessary to know its solubility in different solvents. In this paper, the solubilities of DMMT in water, DMF, methanol, ethanol, 1-propanol, 2-propanol, 1-butanol, and 2-butanol between (293 and 343) K were measured using a laser monitoring observation techninque at atmospheric pressure. The method employed in this work was classed as a synthetic method, which was much faster and more reliable than the analytical method.¹

Experimental Section

Materials. A white crystalline powder of DMMT, purchased from Baiqi Chemical Technology Co., was prepared by recrystallizing from the solution of water two times. Its mass fraction purity determined by HPLC was higher than 99.4 %. Other reagents are analytical research grade reagents from Beijing Chemical Reagent Co.

Apparatus and Procedures. The solubility of DMMT was measured using an apparatus similar to that described in the literature² and described briefly here. A 500 mL jacketed vessel was used to determined the solubility, and the temperature was controlled to be constant (fluctuates with 0.05 K) through a thermostat water bath. The dissolution of the solute was examined by the laser beam penetrating the vessel. To prevent the evaporation of the solvent, a condenser vessel was introduced. The masses of the samples and solvents were weighted using an analytical balance (Sartorius CP224S, Germany) with an uncertainty of \pm 0.0001 g. During experiments, the fluid in the glass vessel was monitored by a laser beam.^{3–6} Predetermined excess amounts of solvent and DMMT of known mass were placed in the inner chamber of the vessel. The contents of the vessel were stirred continuously at a required temperature. In the early stage of the experiment, the laser beam was blocked by the undissolved particles of DMMT in the solution, so the intensity of the laser beam penetrating the vessel was lower. Along with the dissolution of the particles of the solute, the intensity of the laser beam increased gradually. When the solute dissolved completely, the solution was clear, and the laser intensity

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reached maximum. Then additional solute of known mass {about (1 to 5) mg} was introduced into the vessel. This procedure was repeated until the penetrated laser intensity could not return to maximum or, in other words, the last addition of solute could not dissolve completely. The interval of addition was 120 min. The total amount of the solute consumed was recorded. The same solubility experiment was conducted three times, and the mean values were used to calculate the mole fraction solubility (x_1) based on eq 1

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$$x_1 = \frac{m_1 / M_1}{m_1 / M_1 + m_2 / M_2} \tag{1}$$

where m_1 and m_2 represent the mass of the solute and solvent, respectively, and M_1 and M_2 are the molecular weight of the solute and solvent, respectively. The uncertainty of the experimental solubility values is about 0.5 %. The uncertainty in the solubility values can be due to uncertainties in the temperature measurements, weighing procedure, and instabilities of the water bath.

Results and Discussion

The solubilities of DMMT in water, DMF, methanol, ethanol, 1-propanol, 2-propanol, 1-butanol, and 2-butanol between (293 and 343) K are shown in Table 1. The relationship between temperature and solubility of DMMT is correlated with a semiempirical equation⁷

$$\ln x_1 = a + \frac{b}{T} + c \ln T \tag{2}$$

where T is the absolute temperature and a, b, and c are empirical constants. The difference between experimental and calculated results is also presented in Table 1. The values of the three parameters a, b, and c together with the root-mean-square deviations (rmsd) are listed in Table 2. The rmsd is defined as follows

$$\mathrm{rmsd} = \left[\frac{\sum_{j=1}^{N} \left(x_{1,j} - x_{1,j}^{\mathrm{calcd}}\right)^2}{N-1}\right]^{1/2}$$
(3)

where *N* is the number of experimental points; $x_{l,j}^{calc}$ is the solubility calculated from eq 2; and $x_{l,j}$ is the experimental value of solubility.

Solvents between (293 and 343) K							
<i>T</i> /K	$10^4 x_1$	$10^4(x_1 - x_1^{\text{calcd}})$	<i>T</i> /K	$10^4 x_1$	$10^4(x_1 - x_1^{\text{calcd}})$		
		Wa	ater				
293.15	42.12	0.83	323.35	161.2	3.2		
298.12	51.57	-0.04	328.24	198.8	3.0		
303.15	63.65	-0.98	333.35	246.4	1.8		
308.22	80.05	-0.96	338.21	302.6	0.7		
313.35	100.9	-0.8	343.30	370.8	-5.1		
318.28	126.8	0.3					
		DN	МF				
293.45	8.025	0.451	323.20	21.21	0.42		
298.34	8.750	-0.258	328.12	25.28	0.95		
303.35	10.46	-0.26	333.30	29.72	1.09		
308.38	12.21	-0.53	338.22	33.54	0.20		
313.25	14.62	-0.38	345.15	39.32	-1.82		
318.22	17.94	0.26					
		Meth	nanol				
293.05	1.564	-0.007	318.24	3 479	-0.008		
298.17	1 856	0.015	323.25	4 138	0.034		
303.15	2 195	0.043	328.23	4 855	0.024		
308.20	2.175	0.043	333.15	5 712	0.030		
313.05	2.914	-0.035	555.15	5.712	0.050		
	Ed. 1						
202 25	0 5228	0.0072	222 55	1 226	-0.007		
293.23	0.5556	-0.0072	227.45	1.520	-0.007		
298.13	0.0150	-0.0003	327.43	1.333	0.019		
202.93	0.7508	0.0022	220.05	1.015	0.040		
308.10	0.8478	-0.0117	242.20	2.058	-0.003		
312.94	0.9910	-0.0085	342.20	2.205	-0.037		
516.15	1.1//	0.000					
		1-Pro	panol				
293.17	0.5795	-0.0088	323.20	1.610	0.008		
298.14	0.7343	0.0098	328.34	1.762	-0.039		
303.25	0.8518	-0.0289	332.95	1.887	-0.088		
308.12	1.066	0.023	338.18	2.160	-0.008		
313.15	1.265	0.043	343.16	2.406	0.066		
318.23	1.399	-0.012					
		2-Pro	panol				
293.15	0.3471	-0.0104	323.25	0.7958	-0.0107		
298.28	0.4153	0.0058	328.16	0.9088	-0.0151		
303.35	0.4795	0.0107	333.35	1.055	-0.012		
308.14	0.5427	0.0092	338.32	1.229	0.003		
313.25	0.6149	0.0020	343.45	1.441	0.026		
318.20	0.6959	-0.0059					
		1-Bu	tanol				
293.15	0.6108	-0.0079	323.00	1.119	-0.020		
298.21	0.6925	0.0088	328.14	1.261	-0.009		
303.35	0.7655	0.0075	333.05	1.411	0.000		
308.14	0.8492	0.0136	338.12	1.582	0.008		
313.05	0.9473	0.0227	343.10	1.786	0.032		
318.28	1.029	-0.002					
		2-Bu	tanol				
293.35	0.3159	0.0047	323.00	0.7523	0.0226		
298.37	0.3493	0.0096	327.33	0.9183	0.0414		
303.25	0.4116	0.0327	330.85	1.095	0.067		
308.24	0.4365	0.0029	335.57	1.329	0.041		
313.15	0.4842	-0.0215	340.50	1.647	-0.006		

0.0165

318.12

0.6194

Table 1. Mole Fraction Solubility of DMMT x_1 in Different Solvents between (293 and 343) K

Table 2. Parameters of Equation 2 for DMMT in Different Solvents

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а	b	С	10 ⁵ rmsd
-152.55	3168.7	23.985	22.90
-60.612	-273.74	9.5674	8.03
-171.59	4902.0	25.721	0.28
-18.234	-2148.9	2.7654	0.02
281.87	-16000	-41.726	0.42
-141.77	3852.0	20.841	0.12
-122.00	3499.5	17.669	0.16
-681.19	28370	101.05	0.32
	a -152.55 -60.612 -171.59 -18.234 281.87 -141.77 -122.00 -681.19	a b -152.55 3168.7 -60.612 -273.74 -171.59 4902.0 -18.234 -2148.9 281.87 -16000 -141.77 3852.0 -122.00 3499.5 -681.19 28370	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$

From Table 1 and Table 2, we could elicit the conclusions: (1) The solubilities of DMMT in alcohols increase with increase of temperature, but the increment with temperature varies according to different solvents. (2) From Table 2, we could find parameter c in all solvents is relatively small, which is true for many compounds under most conditions, so the last term of eq 2 is neglected in many cases. (3) It can be seen that DMMT dissolved much more in water than in the other seven solvents, and the solubility in 2-butanol is the lowest. (4) All the experimental data can be regressed by eq 2 for solvents. The experimental solubility and correlation equation in this work can be used as essential models in the manufacturing and purifying processes of DMMT in industry.

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